

Table I
 I and I_0 Values Calculated Using Equations 14 and 15 from Data Obtained in Living Isobutylene Polymerizations¹⁷

(a) TMHDIH/BCl₃/DMA/CH₃Cl/IB/-45 °C (ref 17)^a

sampling, min	conv, %	\bar{P}_n	\bar{P}_n^b	\bar{P}_w/\bar{P}_n	I^c	I_0^c
20	25.5	14.6	57	1.36	3.1	3.5
40	56.7	27.1	48	1.16	2.7	3.4
60	73.2	33.2	45	1.15	3.0	4.1
100	91.1	40.6	45	1.14	3.3	5.2
140	93.7	42.1	45	1.14	3.4	5.5
180	96.7	45.1	47	1.12	3.2	5.3
240	98.4	46.2	47	1.12	3.3	5.5

(b) CumOMe/TiCl₄/CH₃Cl (40 vol %)/*n*-Hx (60 vol %)/-80 °C (ref 22)^d

V_0 , mL	\bar{P}_n	\bar{P}_w/\bar{P}_n	I_0^e	[CumOMe], mol/L	[TiCl ₄], mol/L
150	51.7	1.24	12.4	0.073	0.38
300	60.6	1.15	9.1	0.035	0.13
300	68.5	1.12	8.2	0.027	0.12
150	69.5	1.16	11.1	0.021	0.06
150	122.6	1.07	8.6	0.012	0.04

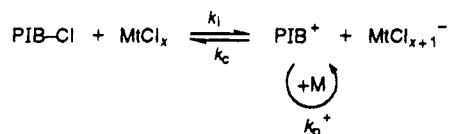
^a $V_0 = 1700$ mL, [BCl₃]₀ = 0.53 mol/L, [M]₀ = 1.57 mol/L (150 g of IB), [DMA]₀ = 0.042 mol/L, [TMHDIH]₀ = 0.042 mol/L. Batch polymerizations with sampling. TMHDIH = 2,4,4,6-tetramethyl-2,6-dihydroxyheptane; DMA = dimethylacetamide; IB = isobutylene.

^b For 100% conversion. ^c The minimum error in these values is ±10% since \bar{P}_w/\bar{P}_n cannot be calculated to better than ±0.1. ^d [M]₀ = 0.6 mol/L of IB; incremental monomer addition (3 × (7 mL of IB/5 min) for $V_0 = 150$ mL and 3 × (14 cm³ of IB/5 min) for $V_0 = 300$ mL); convn = 100%. CumOMe = dicumylmethoxy; IB = isobutylene.

^e The minimum error is ±10%.

narrow MWD polymers ($\bar{M}_w/\bar{M}_n = 1.1$ – 1.2)^{1–5} and are unusually slow; for example, a BCl₃-coinitiated polymerization in the presence of the electron-pair donor dimethylacetamide yielded a degree of polymerization $\bar{P}_n = 46.2$ ($\bar{M}_n = 2600$) in 4 h (!) (Table Ia and ref 17) while TiCl₄ coininitiation produced polymers with $\bar{P}_n = 180$ ($\bar{M}_n = 10\,000$) in 15–30 min, depending on the strength of the electron-pair donor present (Table II and ref 7). Also, “extension” isobutylene polymerizations using chloride-terminated polyisobutylene macroinitiators yielded a $\bar{P}_n = 250$ and bimodal distribution in 10 min in the absence of donors¹¹ and a $\bar{P}_n = 15$ and monomodal, narrow distribution in 15 min in the presence of the strong donor dimethylacetamide.⁵ The large difference in polymerization rates suggests the involvement of chain carriers with different reactivities in the presence and absence of electron-pair donors.

The question arises as to what are the active center chain carriers in living isobutylene polymerizations in the presence of electron pair donors. Let us consider first the case of unpaired ions in a rapid equilibrium with dormant covalent species



The lifetime of the cation will be determined by k_c . The shortest possible lifetime of the active carbocations can be estimated assuming diffusion-controlled collapse with the counteranion ($k_D \sim 10^9$ L mol⁻¹ s⁻¹); thus a $k_c = 10^{10}$ L mol⁻¹ s⁻¹ can be assumed for the rate constant of collapse. The selection of a polymerization rate constant of $k_p^+ = 10^5$ L mol⁻¹ s⁻¹ seems reasonable for this case ($k_p = 10^4$ L mol⁻¹ s⁻¹ for isobutylene, see above, and the most credible

Table II
 Effect of Solvent Polarity in IB Polymerizations Initiated by CumCl/DMA/TiCl₄ (Ref 3)^a

CH ₃ Cl, vol %	<i>n</i> -Hx, vol %	convn, %	\bar{P}_n	\bar{P}_w/\bar{P}_n	I^b	I_0^b
40	60	8	21	1.11	1.7	1.7
60	40	41	105	1.19	10.5	12.9
80	20	100	275	1.13	18.4	36.0
100		100	256	1.21	27.4	54.0

^a [CumCl]₀ = 0.0036 mol/L; [TiCl₄]₀ = 0.066 mol/L; [DMA]₀ = 0.0039 mol/L; [M]₀ = 0.87 mol/L; polymerization time = 10 min. CumCl = cumyl chloride; DMA = dimethylacetamide; IB = isobutylene. ^b The minimum error is ±10%.

values of k_p^+ for styrene in chlorinated solvents of medium dielectric constants ($D \sim 10$ at 300 K) lie in the 10^4 – 10^6 L mol⁻¹ s⁻¹ range.²⁰ From the polymerization rate expression

$$\ln \frac{[M]_0}{[M]} = k_p^+ [P_n^+] t$$

Table I shows conversion–time data for a living isobutylene polymerization in the presence of the strong donor dimethylacetamide taken from ref 17. The $\ln [M]_0/[M]$ – t plot yielded $k_p^+ [P_n^+] = 3.63 \times 10^{-4}$ s⁻¹; with $k_p = 10^5$ L mol⁻¹ s⁻¹ we get $[P_n^+] = 3.63 \times 10^{-9}$ mol/L.

The lifetime of the carbocation, τ , can be calculated as follows:

$$\tau = \frac{[P_n^+]}{k_c [P_n^+] [MtCl_{x+1}^-]} = \frac{1}{k_c [P_n^+]} = 0.026 \text{ s}$$

With [M] = 1.57 mol/L, \bar{P}_n of the polymer formed during the lifetime of the active species, i.e., in 0.026 s, should be

$$\bar{P}_n = k_p^+ [M] \tau = 4100$$

Thus, polymerization assuming unpaired-ion chain carriers with a lifetime of 0.026 s, the shortest possible with reasonable assumptions, gives a \bar{P}_n of 4100 versus the \bar{P}_n of 40.6 found (see Table I). This is certainly a striking difference. If the collapse is viewed to involve the breaking of a covalent bond Cl_xMtCl_x, the rate constant would be in the range of 10^7 L mol⁻¹ s⁻¹,¹⁴ which would yield a longer lifetime and thus an even higher molecular weight polymer. On the basis of the above exercise, we can conclude that the chain carriers in living isobutylene polymerizations in the presence of electron-pair donors are most likely not unpaired ions. If even a small proportion of the polymerization were through unpaired ions, there should be a bimodal distribution with some high molecular weight polymer. This conclusion leaves us with two theoretically possible active species: the covalent species and paired ions.

In the case of an insertion mechanism, the covalent species should be polymerization-active. However, evidence has shown that the tertiary ester or ether/TiCl₄ complexes are inactive in a 1:1 molar ratio.^{2,5} Also, data suggest that tertiary ester, tertiary ether, tertiary chloride + donor, tertiary alcohol + donor, and mixed tertiary ester + tertiary chloride/TiCl₄ initiated polymerizations proceed by the same mechanism,^{3–5,17} and very recently the same conclusion has been reached for isobutylene–diene copolymerizations initiated by tertiary ester and ether/TiCl₄ initiating systems.²¹ All the references cited reported the formation of tertiary chloride capped polymers, regardless of the structure of the initiator used, demonstrating ion exchange at the active sites. These evidences are interpreted to indicate that the covalent species are

not polymerization-active. The ionic mechanism is further supported by the fact that polymerization rates were found to increase with decreasing temperatures.^{21,22}

The above arguments leave us with the conclusion that almost certainly in living isobutylene polymerizations in the presence of certain electron-pair donors the active centers are paired ions.

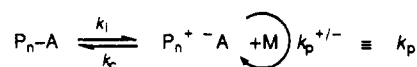
C. Molecular Weight Distribution

Having arrived at the conclusion that living isobutylene polymerizations in the presence of electron-pair donors are characterized by an equilibrium between dormant polyisobutylene-chlorides and active ion pairs, we will derive the molecular weight distribution for these systems.

The MWD in similar living anionic systems, where active and dormant species coexist, was treated by Figini and Schultz.²³ In a treatment given for quasiliving polymerizations²⁴ MWD was discussed in terms of reversible transfer and termination, but the effect of reversible termination was not considered.

Figini and Schultz treated such polymerizations as a series of well-defined successive events, namely, the addition of monomer droplets into a polymerizing mixture.²³ The above authors and later Litt²⁵ used this concept in evaluating the effect of inadequate mixing on the MWD in living anionic polymerizations. We will consider the living cationic polymerization of isobutylene as successive growing periods (productive ionization periods) and derive equations for the MWD for the cases of constant and varying monomer concentrations.

C.1. MWD for Constant Monomer Concentration. In living isobutylene polymerizations characterized by a dynamic equilibrium between dormant polymers and ion pairs



the probability of ion-pair propagation is given as

$$\alpha = \frac{k_p[M][P_n^+]}{k_p[M][P_n^+] + k_c[P_n^+]} = \frac{k_p/k_c[M]}{1 + k_p/k_c[M]} \quad (1)$$

where k_i , k_p , and k_c stand for the initiation, propagation, and collapse rate constants, respectively, $[M]$ stands for the monomer concentration, and $[P_n^+]$ is the ion-pair concentration. If true Poisson growth takes place, then

$$k_p/k_c[M] \ll 1 \quad (2)$$

and the ion pair ionizes and collapses many times per monomer addition, and it is unlikely that more than one monomer unit will be added before a collapse. When the ion pair can add several monomer units before collapsing, the distribution per addition is broadened to the most probable distribution. However, the number of times an active center ionizes and collapses during the course of the polymerization must follow a Poisson distribution for all the active centers. Similarly, the number of times an active center ionizes and adds at least one monomer before collapsing, a productive ionization, must follow a Poisson distribution for all the active centers.

We can define those centers that have ionized productively i times as N_i

$$N_i = \exp(-\bar{z}) \frac{\bar{z}^i}{i!} \quad (3)$$

where \bar{z} is the average number of times the centers ionize

productively. The average degree of polymerization for any population, N_i , is easily defined in terms of α , the probability of propagation (past the first monomer unit) in a productive ionization

$$\bar{P}(1)_n = \frac{1}{1-\alpha}; \quad \bar{P}(1)_w = \frac{1+\alpha}{1-\alpha} \quad (4)$$

where $\bar{P}(1)$ is the average degree of polymerization of those ion pairs per productive ionization. The other average degrees of polymerization can be written²³ as

$$\bar{P}(i)_n = \frac{i}{1-\alpha}; \quad \bar{P}(i)_w = \frac{i+\alpha}{1-\alpha} \quad (5)$$

Since we define the fraction of centers that have ionized productively i times and can write the average $\bar{P}(i)_n$ and $\bar{P}(i)_w$, we can sum those to determine the weight-average and the number-average degrees of polymerization for the whole system

$$\bar{P}_n = \frac{\sum_{i=1}^{\infty} N_i \bar{P}(i)_n}{\sum_{i=1}^{\infty} N_i} \quad (6)$$

where $\bar{P}(i)_n$ is the number-average degree of polymerization of these molecules. Similarly

$$\bar{P}_w = \frac{\sum_{i=1}^{\infty} w_i \bar{P}(i)_w}{\sum_{i=1}^{\infty} w_i} = \frac{\sum_{i=1}^{\infty} N_i \bar{P}(i)_n \bar{P}(i)_w}{\sum_{i=1}^{\infty} N_i \bar{P}(i)_n} \quad (7)$$

From Figini and Schultz²³

$$\bar{P}_n = \sum_{i=1}^{\infty} \exp(-\bar{z}) \frac{\bar{z}^i}{i!} \frac{i}{1-\alpha} = \frac{\bar{z}}{1-\alpha} \quad (8)$$

$$\bar{P}_w = \frac{\exp(-\bar{z}) \sum_{i=1}^{\infty} \frac{\bar{z}^i}{i!} \frac{i}{1-\alpha} \frac{i+\alpha}{1-\alpha}}{\exp(-\bar{z}) \sum_{i=1}^{\infty} \frac{\bar{z}^i}{i!} \frac{i}{1-\alpha}} \quad (9)$$

Equation 9 can be summed to give

$$\bar{P}_w = \frac{\bar{z}^2 + \bar{z}(1+\alpha)}{\bar{z}(1-\alpha)} = \frac{\bar{z}}{1-\alpha} + \frac{1+\alpha}{1-\alpha} = \bar{P}_n + \bar{P}(1)_w \quad (10)$$

When α is very small, eqs 8 and 10 simplify to the normal Poisson distribution. When α approaches 1, several monomer units add at each ionization and the distribution broadens.

The average number of monomer units added per productive ionization is defined in eq 4 and can be called the "run number", \bar{l} . Thus

$$\bar{l} = \frac{1}{1-\alpha} = 1 + k_p/k_c[M] \quad (11)$$

In these terms eq 10 can be rewritten as

$$\frac{\bar{P}_w}{\bar{P}_n} = 1 + \frac{2\bar{l}-1}{\bar{P}_n} \quad (12)$$

Thus, if \bar{P}_n and \bar{P}_w , the number- and weight-average degrees

of polymerization, are known, we can calculate \bar{l} , the average number of monomer units polymerized per productive ionization.

C.2. MWD for Varying Monomer Concentration.

When a batch polymerization is carried out, monomer concentration will drop toward zero as the monomer is consumed. Therefore, α drops toward zero as the polymerization progresses. Since we are discussing living isobutylene polymerizations, initially the polymer could grow in larger jumps while the last portion will grow one unit at a time. This can be taken into account very easily by averaging \bar{l} over the monomer concentration

$$\bar{l} = \frac{\int_{[M]_0}^{[M]} \bar{l} d[M]}{\int_{[M]_0}^{[M]} d[M]} = \frac{\int_{[M]_0}^{[M]} (1 + k_p/k_i[M]) d[M]}{\int_{[M]_0}^{[M]} d[M]} = 1 + \frac{k_p[M]_0 \left(1 + \frac{[M]}{[M]_0}\right)}{2k_c} \quad (13)$$

At complete conversion $[M] = 0$ and $\bar{l} = (\bar{l}_0 + 1)/2$

$$\frac{\bar{P}_w}{\bar{P}_n} = 1 + \frac{2\bar{l} - 1}{\bar{P}_n} = 1 + \frac{\bar{l}_0}{\bar{P}_n} \quad (14)$$

and at intermediate conversions

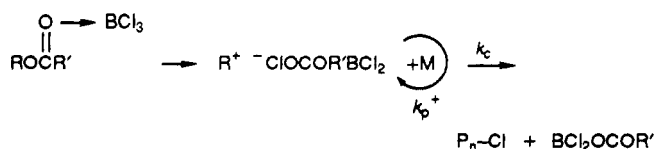
$$\bar{l} = 1 + \frac{\bar{l}_0 - 1}{2} \left(1 + \frac{[M]}{[M]_0}\right) \quad (15)$$

where \bar{l}_0 is the run number at $[M] = [M]_0$.

Figure 1 displays \bar{P}_w/\bar{P}_n plots for various \bar{l} values calculated by using eq 14. The MWD narrows with increasing \bar{P}_n values, and the smaller the \bar{l} , the narrower the MWD for the same \bar{P}_n value. Small \bar{l} values can yield MWDs close to the Poisson values at reasonably high \bar{P}_n .

Living IB polymerizations have often been carried out by using the incremental monomer addition technique.⁸ Incremental monomer addition allows the use of smaller $[M]_0$ compared to a conventional batch polymerization. Smaller $[M]_0$ yields smaller \bar{l}_0 and consequently narrower MWD. MWD can then be minimized by using continuous monomer addition and maintaining low monomer concentration (high conversion). Quasiliving polymerizations^{12,26} conducted under these conditions indeed yielded narrower MWDs than conventional batch polymerizations.

In the next section we will use the above approach to evaluate MWD data available for living IB polymerizations. We find it important to emphasize here that our treatment is not applicable to isobutylene polymerizations initiated by tertiary ester and ether/ BCl_3 where a marked shift in ionization equilibria occurs during initiation and/or propagation, leading to an abrupt change in polymerization rate^{8,9} and in \bar{l} . Those polymerizations are very rapid initially, indicating the involvement of unpaired ions in the initial phase of propagation:



Collapse with the $\text{BCl}_2\text{OCOR}'/\text{Cl}^-$ or $\text{BCl}_2\text{OR}'/\text{Cl}^-$ counteranion, however, yields a tertiary chloride capped polyisobutylene and a donor compound ($\text{BCl}_2\text{OCOR}'$ or $\text{BCl}_2\text{OR}'$) and propagation will proceed by ion pairs.⁵ In these systems the molecular weight distribution of the polymers

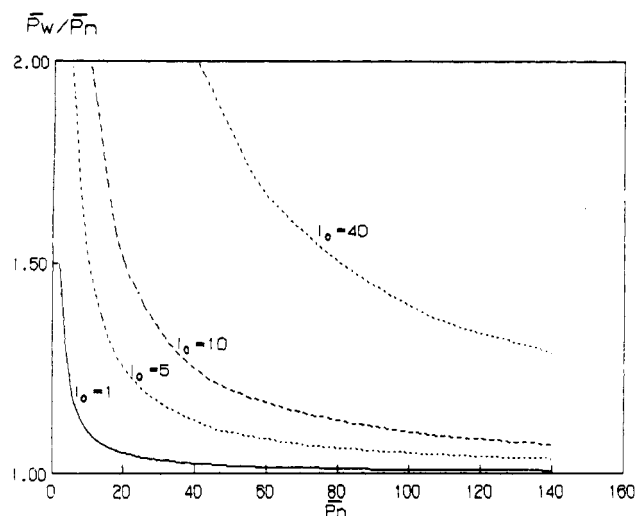


Figure 1. \bar{P}_w/\bar{P}_n vs \bar{P}_n plots for various \bar{l}_0 values.

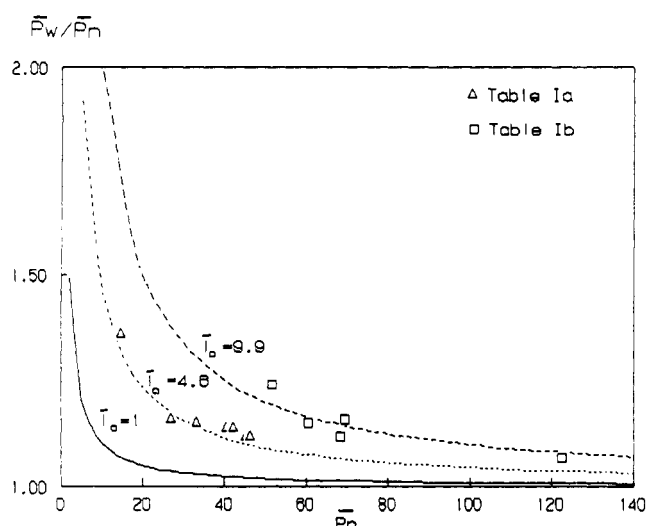


Figure 2. \bar{P}_w/\bar{P}_n vs \bar{P}_n plots for $\bar{l}_0 = 4.6$ and 9.9 calculated from eq 14. Experimental points: (Δ) data in Table Ia; (\square) data in Table Ib.

is relatively broad, as opposed to the narrow distributions obtained in the presence of certain electron-pair donors.

D. Evaluation of MWDs Measured in Living IB Polymerizations in the Presence of Certain Electron-Pair Donors

Table Ia shows \bar{l} and \bar{l}_0 values calculated by using eqs 14 and 15 for a living batch isobutylene polymerization. Assuming free-ion chain carriers, the active center concentration was calculated to be on the order of 10^{-8} mol/L (see section B.1). These active centers would add several thousand units before interacting with the counteranion. This means that no center would react more than once at the relatively low monomer/initiator ratio (Table Ia). We would then expect a high \bar{P}_n initially, which would decrease as the monomer was used up and the chains formed became shorter. The data in Table Ia show that exactly the opposite was found. \bar{l} values are reasonably constant, as expected in the case of living polymerizations. A gradual rise of \bar{l}_0 with conversion in Table Ia may be due to the rise of the dielectric constant of the medium as isobutylene is used up. Table Ib shows living IB batch polymerizations by incremental monomer addition. \bar{l}_0 values calculated using eq 14 are reasonably constant for the same initial monomer concentration ($[M]_0 = 0.6$ mol/L).

Figure 2 shows \bar{P}_w/\bar{P}_n vs \bar{P}_n plots calculated for $\bar{l}_0 = 4.6$ and 9.9 using eq 14. The experimental data points (Table

l) in Figure 2 are in good agreement with the calculated values. In addition, the data in Table Ib reveal that \bar{l}_0 has no dependence on the initiator concentration, confirming ion-pair chain carriers.

Table II shows that \bar{l}_0 increases dramatically with increasing solvent polarity, which is characteristic of ion pairs,²² and reaches $\bar{l}_0 = 54$ for the TiCl_4 -coinitiated polymerization in CH_3Cl . This suggests a higher degree of ion-pair stabilization or a lower collapse rate compared to BCl_3 -coinitiated polymerizations in the same solvent ($\bar{l}_0 = 4.6$; Table Ia).

E. Summary and Conclusions

Several hypotheses were discussed regarding the nature of the active centers in living isobutylene polymerizations in the presence of electron-pair donors. The first was that unpaired ("free") ions participated in the polymerization. On the basis of the observed polymerization rate, the free ion concentration would be on the order of 10^{-8} mol/L and would polymerize several thousand units before interacting with the counteranion. This means that no center would react more than once at the low monomer/initiator ratios used in the isobutylene polymerizations discussed above. We would then expect a high \bar{P}_n initially, which would decrease as the monomer was used up and the chains formed became shorter. Table I shows that exactly the opposite was found.

Even if a small fraction of the polymerization were due to free ions, a different molecular weight distribution would be found; a few percent of high molecular weight polymer would give a very broad distribution. Thus, the narrow MWD and a degree of polymerization that is proportional to conversion under the conditions described in this paper imply that only one species is active and that it has a low-propagation rate constant. Since the covalent species has earlier been shown to be inactive, the active species can only be the ion pair. The lack of dependence of \bar{l}_0 on initiator concentration, Table Ib, verifies that the collapse is a first-order process, and thus the propagation proceeds only through solvated ion pairs.

A gradual rise of \bar{l}_0 with conversion is noted in Table Ia. This could be due to the rise of the dielectric constant of the medium as isobutylene is used up. Table II shows the drastic changes in \bar{l}_0 with the dielectric constant for the $\text{CumCl}/\text{TiCl}_4$ initiating system, which is characteristic of ion pairs. The change in volume due to polymerization of isobutylene will raise the dielectric constant from 11.0 to 11.6. This might raise \bar{l} sufficiently to compensate for the decreasing monomer concentration and raise the calculated value of \bar{l}_0 .

Acknowledgment. Thoughtful comments by Dr. G. J. Wilson and Professor P. H. Plesch are greatly appreciated. We thank Professor Kennedy for his support.

References and Notes

- (1) Kaszas, G.; Puskas, J. E.; Kennedy, J. P. *Polym. Bull.* **1987**, *18* (2), 123.
- (2) Kaszas, G.; Puskas, J. E.; Kennedy, J. P. *Makromol. Chem., Macromol. Symp.* **1988**, *13/14*, 473.
- (3) Kaszas, G.; Puskas, J. E.; Kennedy, J. P.; Chen, C. C. *J. Macromol. Sci., Chem.* **1989**, *A26* (8), 1099.
- (4) Kaszas, G.; Puskas, J. E.; Kennedy, J. P. *Polym. Bull.* **1988**, *20*, 413.
- (5) Kaszas, G.; Puskas, J. P.; Chen, C. C.; Kennedy, J. P. *Macromolecules* **1990**, *23*, 3909.
- (6) Kaszas, G.; Puskas, J. E.; Kennedy, J. P. *J. Appl. Polym. Sci.* **1990**, *39*, 119.
- (7) Kaszas, G.; Puskas, J. E.; Kennedy, J. P.; Hager, W. H. *J. Polym. Sci., Polym. Chem. Ed.*, in press; U.S. Patent 4,946,899, 1990.
- (8) Faust, R.; Kennedy, J. P. *J. Polym. Sci.* **1987**, *A25*, 1847.
- (9) Mishra, M. K.; Kennedy, J. P. *J. Macromol. Sci.* **1987**, *A24* (8), 933.
- (10) Kennedy, J. P.; Kelen, T.; Tudos, F. *J. Macromol. Sci., Chem.* **1982-83**, *A18* (9), 1189.
- (11) Nuyken, O.; Pask, S. D.; Vischer, A.; Walter, M. *Makromol. Chem.* **1985**, *186*, 172.
- (12) Puskas, J. E.; Kaszas, G.; Kennedy, J. P.; Kelen, T.; Tudos, F. *J. Macromol. Sci., Chem.* **1982-83**, *A18* (9), 1229.
- (13) Matyjaszewski, K. IUPAC Preprints, Sympol 90, Paris, 1990, p 69.
- (14) Freyer, C. V.; Nuyken, O. *Makromol. Chem., Macromol. Symp.* **1988**, *13/14*, 319.
- (15) Mayr, H.; Schneider, R.; Grabis, U. *J. Am. Chem. Soc.* **1990**, *112*, 4460.
- (16) Maganini, P. L.; Cesca, S.; Giusty, P.; Priola, A.; Di Maina, M. *Makromol. Chem.* **1977**, *178*, 2235.
- (17) Chen, C. C.; Kaszas, G.; Puskas, J. E.; Kennedy, J. P. *Polym. Bull.* **1989**, *22*, 463.
- (18) Mayr, H. *Makromol. Chem., Macromol. Symp.* **1988**, *13/14*, 43.
- (19) Kennedy, J. P.; Marechal, E. *Carbocationic Polymerization*; Wiley-Interscience: New York, 1982.
- (20) Plesch, P. H. *Cationic Polymerization and Related Processes*; Goethals, E. J., Ed.; Academic Press: London, 1984.
- (21) Kaszas, G.; Puskas, J. E.; Kennedy, J. P., submitted for publication in *Macromolecules*.
- (22) Kaszas, G.; Puskas, J. E.; Kennedy, J. P., unpublished data, 1988.
- (23) Figini, R. V. *Z. Phys. Chem. (Frankfurt)* **1960**, *23*, 224. Figini, R. V.; Schultz, G. V. *Z. phys. Chem. (Frankfurt)* **1960**, *23*, 233; *Makromol. Chem.* **1960**, *41*, 1.
- (24) Kelen, T. *J. Macromol. Sci., Chem.* **1982-83**, *A18* (9), 1339.
- (25) Litt, M. *J. Polym. Sci.* **1962**, *58*, 429.
- (26) Faust, R.; Fehervari, A.; Kennedy, J. P. *J. Macromol. Sci., Chem.* **1982-83**, *A18* (9), 1209.

Registry No. Isobutylene, 115-11-7; isobutylene (homopolymer), 9003-27-4.